

# Hydrogen Confinement in Carbon Nanopores: Extreme Densification at Ambient Temperature

Nidia C. Gallego,<sup>\*,†</sup> Lilin He,<sup>‡</sup> Dipendu Saha,<sup>†</sup> Cristian I. Contescu,<sup>†</sup> and Yuri B. Melnichenko<sup>\*,‡</sup>

<sup>†</sup>Materials Science and Technology Division and <sup>‡</sup>Neutron Scattering Sciences Division, Oak Ridge National Laboratory, Oak Ridge, Tennessee 37831, United States

Supporting Information

**ABSTRACT:** In-situ small-angle neutron scattering studies of H<sub>2</sub> confined in small pores of polyfurfuryl alcohol-derived activated carbon at room temperature have provided for the first time its phase behavior in equilibrium with external H<sub>2</sub> at pressures up to 200 bar. The data were used to evaluate the density of the adsorbed fluid, which appears to be a function of both pore size and pressure and is comparable to the density of liquid H<sub>2</sub> in narrow nanopores at ~200 bar. The surface—molecule interactions responsible for densification of H<sub>2</sub> within the pores create internal pressures that exceed the external gas pressure by a factor of up to ~50, confirming the benefits of adsorptive storage over compressive storage. These results can be used to guide the development of new carbon adsorbents tailored for maximum H<sub>2</sub> storage capacities at near-ambient temperatures.

A critical need in the development of new hydrogen storage media is detailed data on the density of adsorbed  $H_2$  as a function of pore size, pressure, and temperature; however, such measurements have been an experimental challenge. This paper details the use of small-angle neutron scattering (SANS) to provide the first-ever experimental measurements of the phase behavior of  $H_2$  confined in the pores of a carbon adsorbent as a function of pore size and pressure. The results provide evidence that adsorptive gas storage is more efficient at lower pressures and in pores with subnanometer width. The findings suggest a pathway for the synthesis of hydrogen storage materials that exceed U.S. Department of Energy (DOE) targets.

Entrapping  $H_2$  within the nanopores of solid adsorbents by physisorption serves as an alternative option for on-board hydrogen storage for transportation applications.<sup>1-6</sup> The key advantage of the physisorption process for hydrogen storage is the much higher density of the adsorbed gas, which translates into higher storage capacities at lower pressures. The densification of  $H_2$  (or any adsorbed gas in general) is due to the attractive forces between the gas molecules and the pore walls. As a consequence of these interactions, the pressure experienced by the gas molecules confined within the pores can be many times higher than the external gas pressure ( $P_{ext}$ ). Tanaka et al.<sup>7</sup> presented indirect experimental evidence that  $H_2$  confined in singlewalled carbon nanohorns at 20 K is more densely packed than bulk liquid  $H_2$ , with a density approaching that of solid  $H_2$ . In a neutron diffraction study at 77 K, Liu et al.<sup>8</sup> reported that unsaturated metal sites in a metal—organic framework enhance the *surface* packing density of H<sub>2</sub> to values higher than that of solid H<sub>2</sub> at 4 K. Using quantum-chemical calculations and accounting for quantum effects at moderate temperatures, Patchkovskii et al.<sup>9</sup> predicted that H<sub>2</sub> molecules trapped between graphene layers can experience effective internal pressures ( $P_{int}$ ) much higher than  $P_{ext}$  (up to ~55 times higher at  $P_{ext} = 5$  MPa). They also calculated that the pressurization ratio  $P_{int}/P_{ext}$ increases with decreasing temperature and that it is highly dependent on the pore size. These results indicate that the graphene structure acts as a "nanopump" that densifies the confined gas. According to Peng and Morris,<sup>10</sup>  $P_{int}$  and  $P_{ext}$ are related by

$$P_{\rm int} = P_{\rm ext} \exp\left(-\frac{\Delta H}{RT}\right) \tag{1}$$

where  $\Delta H < 0$  is the enthalpy of adsorption, *R* is the gas constant, and T is the temperature. Equation 1 is equivalent to setting the chemical potentials of the external and adsorbed gases equal and using pressure as an approximation for fugacity. Thus, at room temperature,  $|\Delta H|$  must be ~7.5 kJ/mol to increase  $P_{int}$  by an order of magnitude (15 kJ/mol for 2 orders of magnitude). Since the adsorption potential in nanopores, and thus the densification factor, depends strongly on the width of the pores and the pressure, knowledge of the structural characteristics of the materials is crucial in selecting and/or designing the adsorbents for efficient hydrogen storage. First-principles calculations and Monte Carlo simulations have suggested that narrow micropores with subnanometer pore widths (6-7 Å; herein called)nanopores) are the most effective for entrapping  $H_2$  molecules.<sup>11–13</sup> Adsorption measurements<sup>14,15</sup> have confirmed that carbons with median pore widths of 6-7 Å exhibited the highest H<sub>2</sub> adsorption capacity; an average density for the adsorbed H<sub>2</sub> was calculated<sup>15</sup> by assuming that all molecules dwelled within the pores of a particular median width. However, assuming a single density value for adsorbed H<sub>2</sub> is an oversimplification that does not describe the local density in pores of varying sizes in a carbon with a wide pore size distribution.

Detailed information on the adsorbed phase density within pores of various sizes is a critical prerequisite for designing and developing the next generation of hydrogen storage materials; controlling the size and number of pores may lead to improved storage capacity and heat of adsorption. However, acquiring quantitative data on the density of adsorbed  $H_2$  has

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Figure 1. SANS patterns from PFAC under vacuum and at elevated pressures of  $H_2$  at room temperature (raw data before correction for incoherent background). Scattering from bulk  $H_2$  measured at the same pressures as the confined  $H_2$  is also shown. Fitted values of the incoherent background at each pressure are shown at the right. The observed significant differences between the scattering from bulk  $H_2$  and  $H_2$ -loaded carbon are due to the extreme hydrogen densification in small pores. All curves are color-coded.

remained an outstanding challenge because of numerous experimental complications. Recent studies have demonstrated that SANS can provide unique pore-size-specific information on the phase behavior of confined fluids and may be used to evaluate the density of the adsorbed fluid in pores of various sizes, including subnanometer length scales. To date this new methodology has been used to investigate the adsorption of supercritical  $CO_2$  in engineered and natural porous materials such as silica aerogels and coal.<sup>16–18</sup> In this work, we extended the methodology to evaluate for the first time the density of adsorbed H<sub>2</sub> gas in the nanopores and mesopores of polyfurfuryl alcohol-derived activated carbon (PFAC). Furthermore, using an equation of state for H<sub>2</sub>, we calculated the corresponding internal pressures experienced by the confined fluid.

The PFAC material was synthesized following a variation of the procedure of Burket et al.<sup>19</sup> and had a surface area of  $1530 \text{ m}^2/\text{g}$  and a pore volume of 0.68 cm<sup>3</sup>/g, of which 90% was contained in micropores with widths of <20 Å. Synthesis and characterization details may be found in the Supporting Information (SI).

In-situ high-pressure SANS studies were conducted using the general-purpose SANS instrument at Oak Ridge National Laboratory (ORNL),<sup>20</sup> with a neutron wavelength ( $\lambda$ ) of 4.8 Å ( $\Delta\lambda/\lambda \approx 0.13$ ). The sample-detector distance was chosen to cover an overall range of scattering vectors (Q) of 0.01 Å<sup>-1</sup> < Q < 0.8 Å<sup>-1</sup>, where  $Q = (4\pi/\lambda) \sin(\theta/2)$ , in which  $\theta$  is the scattering angle. The upper limit of Q,  $Q_{max} = 0.8$  Å<sup>-1</sup>, was determined by the acceptance angle of a newly built pressure cell. This limit exceeds the upper cutoff of the pressure cell used in our previous studies by a factor of 4.<sup>16-18,21</sup> Thus, the new pressure cell extends the pore sizes (L) accessible to SANS into the subnanometer



**Figure 2.** Ratios of coherent intensities measured for H<sub>2</sub>-loaded and blank (under vacuum) carbon,  $I_{\rm coh}(Q, P)/I_{\rm coh}(Q, P = 0)$ . The Q values (and corresponding pore sizes) selected for density calculations are also shown.

region:  $L \approx 2\pi/Q_{\text{max}} \approx 9$  Å. A powder PFAC sample was outgassed overnight at 300 °C, loaded into a thin-walled aluminum container with an internal thickness of 1 mm, and subsequently mounted inside the high-pressure cell. The H<sub>2</sub> pressure was varied from vacuum up to  $\sim$ 200 bar using a home-built pressure intensifier, and all of the measurements were conducted at room temperature ( $\sim$ 23 °C). The scattering patterns were corrected for detector efficiency, electronic noise, and scattering from the empty pressure cell. The twodimensional scattering patterns were radially averaged and put on an absolute scale [cross section I(Q) in cm<sup>-1</sup>] by means of precalibrated secondary standards. The scattering patterns from the PFAC under vacuum and at different  $H_2$  pressures (Figure 1) show that I(Q) increases continuously with pressure for all values of the scattering vector. The observed variation of I(Q) is due to the cumulative effect of the densification of the adsorbed H<sub>2</sub> in pores and the increasing incoherent background from H<sub>2</sub> with pressure.

The pressure-dependent contribution of the incoherent background  $(I_{inc})$  was determined by fitting the experimentally measured functions I(Q) at each pressure to the Debye equation:<sup>22</sup>

$$I(Q) = \frac{B}{\left(a^{-2} + Q^2\right)^2} + I_{\rm inc}$$
(2)

where *B* is a pressure-dependent variable that accounts for the strong variation of the scattering-length density of H<sub>2</sub> with pressure and *a* is the Debye correlation length in the autocorrelation function of the scattering-length density fluctuations  $\gamma(r) = \exp(-r/a)$ ; a is independent of pressure for completely saturated pores. The fits were performed over the range Q > 0.1 Å<sup>-1</sup>, and the obtained values of  $I_{\rm inc}$  (Figure 1) were subtracted from the experimentally measured intensities to provide the coherent cross sections  $I_{\rm coh}(Q)$ . As explained in the SI, the density of H<sub>2</sub> in the pores ( $\rho_{\rm H_2}$ )<sub>pore</sub> at different values of Q (or, equivalently, at different pore sizes  $L \approx 2\pi/Q$ ) can be evaluated using the ratios of the coherent intensities measured for H<sub>2</sub>-loaded and blank carbons [ $I_{\rm coh}(Q, P)$  and  $I_{\rm coh}(Q, P = 0)$ , respectively]:

$$\frac{I_{\rm coh}(Q, P)}{I_{\rm coh}(Q, P=0)} = \left[1 + 5.6(\rho_{\rm H_2})_{\rm pore}\right]^2$$
(3)



Figure 3. Room-temperature densities of adsorbed  $H_2$  as functions of (A) pressure for selected pore sizes and (B) pore size at constant pressures.

The ratios of coherent intensities under vacuum and at various P are plotted in Figure 2 for the Q range of interest. Six Q values corresponding to maxima in the pore size distribution profile of the PFAC sample (shown in the SI) were selected for density calculations and are noted in Figure 2. The corresponding errors in the coherent intensity ratios (estimated after reduction of the raw data) are also shown. These errors were used to calculate subsequent errors in the density, the densification factor, and  $P_{int}$  using error propagation theory.

The densities of H<sub>2</sub> in carbon pores calculated using eq 3 are plotted in Figure 3A as functions of pressure for the selected pore sizes. The densities of liquid H<sub>2</sub> at the triple point and gaseous H<sub>2</sub> at the corresponding pressures at room temperature are also shown for comparison. It is evident that at room temperature, for any given values of  $P_{\text{ext}}$  and pore size, the density of confined H<sub>2</sub> is considerably higher than that of the bulk gas and approaches the density of liquid H<sub>2</sub> at the highest pressure for the narrowest pore studied. The effect of pore size on the density at constant pressure is clearly illustrated in Figure 3B: the density is systematically higher in the narrow pores and decreases with increasing pore size, reaching almost constant values in the mesoporous range (>20 Å). These results clearly demonstrate the advantage of adsorptive storage over compressed gas storage and emphasize the greater efficiency of micropores over mesopores in the adsorption process.



Figure 4. Room-temperature densification factors of adsorbed H<sub>2</sub> at different external pressures.



**Figure 5.** Internal H<sub>2</sub> pressures within PFAC nanopores derived from room-temperature density values of adsorbed H<sub>2</sub> as a function of  $P_{\text{ext}}$ .  $P_{\text{int}}$  values predicted using the model of Patchkovskii et al.<sup>9</sup> at 50 and 100 bar are also shown for comparison.

The densification factors (i.e., the ratio of the adsorbed and bulk gas densities) at various pressures at T = 23 °C are shown in Figure 4. The ratio is higher at the lowest pressures (40–50 times higher than the bulk density) and decreases with pressure. The decreasing trend of  $P_{\text{int}}$  with increasing  $P_{\text{ext}}$  is a consequence of the nonequivalence of adsorption sites: the strongest binding sites (where the local  $P_{\text{int}}$  is the highest) are occupied first (at low  $P_{\text{ext}}$ ), while the weaker binding sites (with low  $P_{\text{int}}$ ) contribute to adsorption only at higher  $P_{\text{ext}}$ .

As discussed earlier, the overlap of the potentials of opposite walls in nanoscale pores induces extensive densification of the confined fluid, greatly exceeding the fluid density next to an open flat surface. This effect is equivalent to developing an effective "internal" pressure in carbon pores that may exceed by orders of magnitude the external pressure applied to the system.<sup>9–12</sup>To quantify this effect of confinement, we calculated the effective internal pressure corresponding to each H<sub>2</sub> density in pores using the nonideal equation of state for H<sub>2</sub>.<sup>23</sup> The results in Figure 5 demonstrate that  $P_{int}$  within the 9 Å pores varies between 240

and 2400 bar as  $P_{\text{ext}}$  increases from 5 to 207 bar. The difference between  $P_{\text{int}}$  and  $P_{\text{ext}}$  decreases with  $P_{\text{ext}}$  as well as with the pore size, in general agreement with theoretical predictions<sup>9</sup> (Figure 5). However, the variation of the experimentally observed  $P_{\text{int}}$  as a function of pore size is less pronounced than predicted,<sup>9</sup> reflecting the fact that theoretical predictions depend greatly on the strength of the adsorption interactions assumed in the calculations.

Although various theoretical models consistently predict that H<sub>2</sub> adsorption occurs preferentially in the nanopores of solid adsorbents,<sup>11-13,24</sup> providing experimental evidence for such behavior is not possible using "traditional" volumetric or gravimetric adsorption methods. The results reported here represent the first experimental characterization of the phase behavior of H<sub>2</sub> confined in the pores of a carbon adsorbent as a function of pore size and pressure. They provide experimental evidence that adsorptive gas storage is more efficient at low pressures than at elevated pressures and that the adsorption process occurs most effectively in small pores. To put these findings into perspective, if a carbon adsorbent containing  $1 \text{ cm}^3/\text{g}$  of pores with widths of only 9 Å could be synthesized, the amount of H<sub>2</sub> that could be stored at room temperature and 207 bar would be 8.13 wt %. This uptake (material-based) may approach the DOE system-based target for 2010 (4.5 wt %).<sup>1</sup> We hope that these findings will provide new guidance for the synthesis of porous carbons with tailored/optimized structures and initiate further theoretical considerations explaining fluid densification far away from the liquid-gas critical point.

## ASSOCIATED CONTENT

**Supporting Information.** Detailed synthesis of PFAC, characterization details, and model equations for SANS. This material is available free of charge via the Internet at http://pubs. acs.org.

### AUTHOR INFORMATION

Corresponding Author gallegonc@ornl.gov; melnichenkoy@ornl.gov

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